

**FLOWSERVE**

***Vogt Valves***

***Vogt Valves***

*The Connection Bulletin for  
Fugitive Emissions  
A Leakage Viewpoint*

*CB 12*

# Fugitive Emissions: A Leakage Viewpoint

Guy A. Jolly, P.E.  
 Chief Engineer  
 Vogt Valve Division  
 Edward Vogt Valve  
 Company

### Abstract

Equipment fugitive emissions has created a new acronym — PPM(v) (parts per million, volumetric). This paper is an update of the author's earlier paper "A Treatise on Leakage" but specific to fugitive emissions and the PPM(v)'s leakage acronym. The paper presents how PPM leakage can be correlated with traditional "bubbles" of leakage and how the basic laminar leakage equations can be applied to EPA's list of hazardous air pollutants to project comparative leakage using air and water leakage as the practical standard.



\*Paper available from Vogt Valves.  
 \*\*Re=Reynolds Number

### About the Author

Mr. Jolly is Chief Engineer of the Valve Division of Vogt Valves. He is a registered professional engineer in the State of Kentucky. He holds a BS degree in Mechanical Engineering from the University of Kentucky and a MA degree in Mathematics from the University of Louisville.

He is active in the American Society of Mechanical Engineers (ASME), the American Petroleum Institute (API), the Valve Manufacturers Association (VMA), and the Manufacturing Standardization Society of the Valve and Fitting Industry (MSS). He is a member of ASME B 16 and B31 Main Committees and is Chair of ASME B 16-Subcommittee F. He serves on API Refinery Subgroups on Gate Valves and Quality. He currently serves as President of MSS.

### Background

In the author's paper, "A Treatise on Leakage" theoretical equations were developed that can be used to compare liquid and gas flow rates across leak paths in the laminar flow mode. The laminar flow mode was defined as flow in conduits in which the  $Re \leq 2000$ \*\* It was shown that laminar flow can be characterized as flow that emanates from leak paths in "drops" or in "bubbles" of leakage. For convenience, the basic laminar leakage equations presented in "A Treatise on Leakage" are presented here as follows:

#### EQUATION #1 LIQUID FLOW ACROSS LEAK PATH

$$Q_L = 169273 K_L \frac{\Delta P}{\mu_L}$$

#### EQUATION #2 GAS LEAKAGE ACROSS LEAK PATH

$$Q_g = 11515 \frac{K_L \Delta P P'_a}{\mu_g}$$

#### EQUATION #3 COMPARATIVE GAS/LIQUID ACROSS SAME LEAK PATH

$$\frac{Q_g}{Q_L} = .068 P'_a \left( \frac{\mu_L}{\mu_g} \right)$$

### Nomenclature

- $Q_L$  = Leakage rate of liquid across a leak path, in cubic inches per second at flowing conditions.
- $Q_g$  = Leakage rate of gas across a leak path, in cubic inches per second at standard conditions (14.7 psia @ 60°F)
- $K_L$  = Resistance coefficient for leak path for use in laminar flow equation.
- $\Delta P$  = Differential pressure across capillary/pipe or leak path, in psi.
- $P'_a$  = Average pressure across a leak path, in pounds per square inch absolute (psia).
- $M_U \mu$  = Absolute (dynamic) viscosity, in centipoise.
- $\mu_L$  = Viscosity of liquid in centipoise.
- $\mu_g$  = Viscosity of gas in centipoise.

# Fugitive Emissions: A Leakage Viewpoint

TABLE 1

Size (Spherical)	Volume (1) Drop/Bubble	Leak Rate (SCIS) (2) (3)										
		Drops/Bubbles per Minute										
Drop or Bubble Diameter	In <sup>3</sup>	4	5	6	8	10	16	20	25	32	50	64
1/32"	1.598 x 10 <sup>-5</sup>	1.06 x 10 <sup>-6</sup>	1.33 x 10 <sup>-6</sup>	1.59 x 10 <sup>-6</sup>	2.13 x 10 <sup>-6</sup>	2.66 x 10 <sup>-6</sup>	4.26 x 10 <sup>-6</sup>	5.33 x 10 <sup>-6</sup>	6.65 x 10 <sup>-6</sup>	8.52 x 10 <sup>-6</sup>	1.33 x 10 <sup>-5</sup>	1.70 x 10 <sup>-5</sup>
1/16"	1.278 x 10 <sup>-4</sup>	8.52 x 10 <sup>-6</sup>	1.06 x 10 <sup>-5</sup>	1.28 x 10 <sup>-5</sup>	1.70 x 10 <sup>-5</sup>	2.12 x 10 <sup>-5</sup>	3.41 x 10 <sup>-5</sup>	4.24 x 10 <sup>-5</sup>	5.30 x 10 <sup>-5</sup>	6.82 x 10 <sup>-5</sup>	1.06 x 10 <sup>-4</sup>	13.64 x 10 <sup>-4</sup>
3/32"	4.314 x 10 <sup>-4</sup>	2.88 x 10 <sup>-5</sup>	3.60 x 10 <sup>-5</sup>	4.32 x 10 <sup>-5</sup>	5.76 x 10 <sup>-5</sup>	7.20 x 10 <sup>-5</sup>	1.15 x 10 <sup>-4</sup>	1.44 x 10 <sup>-4</sup>	1.80 x 10 <sup>-4</sup>	2.30 x 10 <sup>-4</sup>	3.60 x 10 <sup>-4</sup>	4.60 x 10 <sup>-4</sup>
1/8"	1.023 x 10 <sup>-3</sup>	6.82 x 10 <sup>-5</sup>	8.52 x 10 <sup>-5</sup>	1.02 x 10 <sup>-4</sup>	1.36 x 10 <sup>-4</sup>	1.71 x 10 <sup>-4</sup>	2.73 x 10 <sup>-4</sup>	3.42 x 10 <sup>-4</sup>	4.26 x 10 <sup>-4</sup>	5.45 x 10 <sup>-4</sup>	8.52 x 10 <sup>-4</sup>	1.09 x 10 <sup>-3</sup>
5/32"	1.997 x 10 <sup>-3</sup>	1.33 x 10 <sup>-4</sup>	1.66 x 10 <sup>-4</sup>	2.00 x 10 <sup>-4</sup>	2.66 x 10 <sup>-4</sup>	3.33 x 10 <sup>-4</sup>	5.32 x 10 <sup>-4</sup>	6.66 x 10 <sup>-4</sup>	8.30 x 10 <sup>-4</sup>	1.06 x 10 <sup>-3</sup>	1.66 x 10 <sup>-3</sup>	2.12 x 10 <sup>-3</sup>
3/16"	3.451 x 10 <sup>-3</sup>	2.30 x 10 <sup>-4</sup>	2.88 x 10 <sup>-4</sup>	3.45 x 10 <sup>-4</sup>	4.6 x 10 <sup>-4</sup>	5.75 x 10 <sup>-4</sup>	9.2 x 10 <sup>-4</sup>	1.15 x 10 <sup>-3</sup>	1.44 x 10 <sup>-3</sup>	1.84 x 10 <sup>-3</sup>	2.88 x 10 <sup>-3</sup>	3.68 x 10 <sup>-3</sup>

1) Volume of drop or bubble =  $\frac{\pi}{6}$  (diameter)<sup>3</sup>

2) SCIS = Standard Cubic Inch per Second Leakage

$$\text{Leakage Rate (SCIS)} = \left( \frac{\text{No. Drops or Bubbles}}{\text{Minute}} \right) \times \left( \frac{\text{Vol. (Drop/Bubble) (In}^3\text{)}}{1} \right) \times \left( \frac{\text{Minute}}{60 \text{ Secs.}} \right)$$

3) Standard in SCIS refers to the collection of bubbles in gas-under-water type tests in which the visible bubble is observed or collected at standard conditions — 14.7 psia @ 60°F. Since the volume of a leaking liquid does not change across a leak path, the leak rates noted above are equal to cubic inches/sec. when referring to liquid leakage rates.

# Fugitive Emissions: A Leakage Viewpoint

Various rates and sizes of “drops” and “bubbles” per minute were quantified in a leakage table which is also included here for convenience (see Table 1).

## Fugitive Emissions

The purpose of this paper is to update the “A Treatise on Leakage” paper as it relates to leakage of the hazardous air pollutants (HAPS) and to correlate the fugitive emissions PPM(V) leakage rates to the traditional “bubbles” of leakage presented in the earlier paper.

Since the “A Treatise on Leakage” paper was published, the issue of *fugitive emissions* has emerged. Fugitive emissions in the context of this paper is defined as follows:

Fugitive emissions is the loss of VOCs (volatile organic compounds)\* through sealing mechanisms separating process fluid from the environment. Fugitive emissions is also referred to as *equipment leaks*. The equipment includes pumps, valves, compressors, pressure relief devices, open-ended valves or lines, flanges, or connectors used within a processing plant.

In short, fugitive emissions is nothing more than equipment leakage of certain fluids but a new term to report its intensity has emerged. This new term is PPM(v) — parts per million volumetric.

Since it may not be readily evident from Equations 1, 2 and 3, the following leakage comparisons are summarized:

Across any given leak path the volumetric leakage rate of a gas will be much greater than for a liquid. This is due to the fact that the viscosity of gases is much less than liquids and the compressibility of gases

allows it to emanate from a leak path to the atmosphere at its greatest natural volume. Liquids being incompressible do not grow in volume as they move across a leak path to the atmosphere. Equations 1 and 2 indicate the leakage rate is inversely proportional to the fluid viscosity. Since liquids have larger viscosities than gases, liquid flow leakage is projected to be less across a given leak path. Equation 2 indicates that a gas leakage across a given leak path is a function of  $\Delta P \times P_a$  while leakage rate for a liquid from Equation 1 is a function of  $\Delta P$  only. This pressure factor influence on leakage may not be evident but it emerges from the theoretical consideration that a gas under higher pressure entering and moving isothermally across a leak path will emerge at atmospheric pressure, much greater than its starting volume while an incompressible liquid leakage volume would not significantly increase upon emerging to the atmosphere.

Water and air have been used for years as test fluids in the equipment industry for testing of products. From this longtime practice, flow from a leak path characterized as “drops” or “bubbles” per minute has been historically used to quantify leakage. Applying Equation 3 to an air versus water leakage calculation would clearly show that air with its lower viscosity would leak at a much greater volumetric rate than water across the same leak path at the same  $\Delta P$ . It can also be shown that an air test at a lower  $\Delta P$  would show more leakage (bubbles) across the same leakage path than water leakage (drops) at a higher  $\Delta P$  water test.

Using water and air as benchmarks for leakage across leak paths, Equations 1 and 2 can be used to compare the relative leakage rates

**Figure 1**

**DFE = Fugitive Emission Flow Rate - SCCM**  
**PFR = Pure Air Flow Rate - SCCM**  
**CFR = Contaminated Air Flow Rate - SCCM**  
**CFR = PFR + DFE**  
**(SCCM = Standard Cubic Centimeter per Minute)**

What is the resultant theoretical volumetric parts per million (PPMV) of a CFR resulting from the introduction of a small volatile organic contaminant (VOC) AFE flow rate into a pure air flow (PFR) stream?

**(NOTE: A typical AFE is small compared to the PFR and can be dropped from the denominator of the following equation without making a significant result on the calculation.)**

$$PPM = \frac{\Delta FE}{PFR} \times \frac{10^6}{10^6}$$

$$PPM = \frac{\Delta FE \times 10^6}{PFR} \times \left( \frac{1}{10^6} \right)$$

$$PPM = \frac{\Delta FE \times 10^6}{PFR} \times \left( \frac{1}{\text{MILLION}} \right) = \frac{\text{PARTS CONTAMINANT PER MILLION}}{\text{MILLION}}$$

TYPICAL CALCULATION:

$\Delta FE = 1 \text{ SCCM}$   
 $PFR = 2 \text{ liters/minute or } 2000 \text{ SCC/minute}$

$$PPMV = \frac{1 \times 10^6 \text{ SCCM}}{2000 \text{ SCCM}} = 500$$

\*Volatile Organic Compound (VOC) is any compound containing the element carbon, excluding methane, carbon monoxide, carbon dioxide, carbonic acid, metallic carbides or carbonates, ammonium carbonate and exempt compounds. (From SCAQMD Rule 1173, amended 12/7/90)

## Fugitive Emissions: A Leakage Viewpoint

of a number of the hazardous air pollutants (HAPs). The Environmental Protection Agency (EPA) has a published listing of those compounds that are currently considered hazardous.

Table 2 represents the leakage rate multiplier determined from Equation 1 that could be used for a number of HAPs when in liquid state. Using water leakage as the base (1.00), Table 3 would indicate that benzene would leak at a rate 9.8 times greater than air across a given leak path at the same  $\Delta P$ .

Table 3 represents the leakage rate multiplier determined from Equation 2 that can be used for a number of the HAPs when in gas/vapor state. Using air leakage as the base (1.00), Table 3 would indicate that benzene would leak at a rate 2.34 times greater than air across a given leak path at the same  $\Delta P$ .

Table 4 is an extensive listing of the viscosities of many of the EPA listed hazardous pollutants. These viscosities can be used with Equations 1, 2 or 3 to establish their relative intensity to leak versus other fluids in the table or the traditional test fluids with viscosities listed in Table 4A.

The PPM(v) leakage indicator has emerged as the most practical measurement method for fugitive emissions leakage. It has been promoted by organic vapor analysis (OVA) instruments that have been developed over the years that have the capability to continuously pump a sample of the atmosphere surrounding equipment through its internal analyzer to detect any trace of VOCs that get into that flow stream. The OVA instruments give the concentration of the VOC in the flow stream in terms of PPM(v) (parts per million, volumetric). Thus, fugitive emissions (equipment leakage) has a new term for leakage. But this

**TABLE 2**
**Hazardous Air Pollutants  
LIQUIDS  
Relative Leakage Rates\***

HAP	LEAKAGE MULTIPLIER
Ammonia	9.80
Vinyl chloride	5.16
Formaldehyde	4.90
1,3 Butadiene	4.26
Ethylene oxide	3.92
Hexane	3.16
Chlorine	2.97
Phosgene	2.51
Methyl ethyl ketone	2.39
Toluene	1.78
Methanol	1.78
Trichloroethylene	1.63
Xylene	1.69
Benzene	1.63
Styrene	1.40
Cumene	1.32
Ethylene dichloride	1.13
*Water	1.00
Carbon tetrachloride	.98

**NOTE:** The viscosity of liquids decrease with increasing temperatures and are negligibly affected by pressure.

\*Based on viscosities at 68°F or 78°F.

**TABLE 3**
**Hazardous Air Pollutants  
(VAPORS/GASES)  
Relative Leakage Rates\***

HAP	LEAKAGE MULTIPLIER
Cumene	2.86
Styrene	2.77
Xylene	2.77
Hexane	2.65
Toluene	2.59
Methyl ethyl ketone	2.46
1, 3 Butadiene.	2.40
Benzene	2.34
Ethylene glycol	2.31
Ethylene dichloride	2.25
Ethylene oxide	1.91
Trichloroethylene	1.94
Carbon tetrachloride	1.86
Methanol	1.84
Formaldehyde	1.80
Ammonia	1.80
Vinyl chloride	1.68
Phosgene	1.53
Hydrogen sulfide	1.50
Chlorine	1.38
*Air	1.00

**NOTE:** The viscosity of gases/vapors increase with increasing temperature and are negligibly affected by pressure.

\*Based on viscosities at 68°F or 78°F.

## Fugitive Emissions: A Leakage Viewpoint

PPM(v) leakage can be theoretically correlated with "bubbles" of leakage by calculating the PPM(v) concentration the "bubbles" of leakage from Table 1 would have it introduced into a typical flow stream of 2 liters/minute. Table 1A relates the correlation of PPM(v) fugitive emissions to bubbles of leakage. (See Figure 1).

As an example, Table 1A indicates that if the volumetric flow rate equal to 6 bubbles/minute ( $\frac{1}{8}$ " bubble size) of pure methane is introduced into a 2 liters/minute flow stream and thoroughly mixed, a theoretical 50 PPM methane flow system would result. The highly used 10,000 PPM fugitive emissions standard for an equipment leak is so large that they are not illustrated in the table. This may mean the leak rate is so large that it is not in the laminar flow range. Other commonly used benchmarks of fugitive emissions leakage, 100 PPM and 500 PPM, can be correlated with "bubbles" of leakage in the table at various "bubbles" sizes.

The 100 PPM and 500 PPM fugitive emissions leakage standard are projected as laminar type leaks due to their correlation with "bubbles" of leakage in Table 1A.

### Summary

This paper has presented the basic laminar flow leakage equations. From these equations, a comparative leakage propensity of several hazardous air pollutants can be determined. The data suggests many of the HAPs with their low viscosity will be more difficult to contain than air or water traditionally used to pressure test equipment. The PPM(V) acronym for fugitive emissions has been correlated with traditional "bubbles" of leakage in a table that would suggest that fugitive emissions standards, 100 PPM, 500 PPM and 1000 PPM are truly in the laminar flow region.

**TABLE 4A**  
**VISCOSITIES OF TYPICAL TEST FLUIDS**

Fluid	Viscosity Gas/Vapor Centipoise
Air	0.018 CP @ 60°F
Freon 114	0.015 CP @ 80°F
Helium	0.020 CP @ 70°F
Methane	0.011 CP @ 70°F
Nitrogen	0.018 CP @ 70°F
Propane	0.008 CP @ 32°F
Steam	0.013 CP @ 212°F
Fluid	Viscosity Liquids Centipoise
Kerosene	2.10 CP @ 60°F
Water	1.13 CP @ 60°F

  

**COMMON LIQUID DATA**

Viscosity Air @ 25°C = 180 MP  
 Viscosity Water Vapor @ 100°C = 130 MP  
 Viscosity Water @ 20°C = .98 CP or 9800 MP  
 Viscosity Propane Liquid @ 20°C = .12 CP  
 Viscosity Propane Vapor @ 20°C = 80 MP

  

**CONVERSION FACTORS**

0°C = 32°F  
 20°C = 68°F  
 25°C = 77°F

50 Micropoise = 0.005 Centipoise  
 90 Micropoise = 0.009 Centipoise  
 100 Micropoise = 0.010 Centipoise  
 200 Micropoise = 0.020 Centipoise  
 1000 Micropoise = 0.10 Centipoise  
 10000 Micropoise = 1.00 Centipoise

# Fugitive Emissions: A Leakage Viewpoint

**TABLE 4**  
**HAZARDOUS AIR POLLUTANT VISCOSITIES**

Hazardous Air Pollutants (1)	Vapor Viscosity Micropoises	Liquid Viscosity Centipoise
Acetaldehyde	85 MP @ 25°C	.22 CP @ 20°C
Acetonitrile	58 MP @ 25°C	.35 CP @ 25°C
Acrolein	80 MP @ 20°C	.36 CP @ 20°C
Acrylic acid	63 MP @ 25°C	.87 CP @ 25°C
Ammonia (2)	100 MP @ 20°C	.10 CP @ 25°C
Aniline	69 MP @ 25°C	2.4 CP @ 40°C
Benzene (including benzene from gasoline)	77 MP @ 25°C	.60 CP @ 20°C
Benzyl chloride	65 MP @ 25°C	1.27 CP @ 25°C
1,3-Butadiene	75 MP @ 20°C	.23 CP @ 20°C
Carbon disulfide	104 MP @ 25°C	.34 CP @ 25°C
Carbon tetrachloride	97 MP @ 20°C	.97 CP @ 20°C
Chlorine (2) (3)	130 MP @ 20°C	.33 CP @ 20°C
Chlorobenzene	75 MP @ 25°C	.76 CP @ 25°C
Chloroform	100 MP @ 20°C	.58 CP @ 20°C
Cumone	63 MP @ 25°C	.74 CP @ 25°C
Dimethyl formamide DMF	60 MP @ 25°C	.80 CP @ 25°C
Epichlorohydrin (1-Chloro-2,3-Epoxybutane)	83 MP @ 20°C	1.25 CP @ 20°C
Ethyl acrylate	70 MP @ 25°C	.53 CP @ 25°C
Ethyl benzene	68 MP @ 25°C	.64 CP @ 25°C
Ethyl chloride (Chloroethane)	95 MP @ 20°C	28 CP @ 20°C
Ethylene dibromide (Dibromoethane)	125 MP @ 50°C	1.7 CP @ 20°C
Ethylene dichloride (1,2-Dichloroethane)	80 MP @ 20°C	.87 CP @ 20°C
Ethylene glycol	78 MP @ 25°C	117.0 CP @ 25°C
Ethylene oxide	94 MP @ 25°C	.25 CP @ 25°C
Formaldehyde	100 MP @ 25°C	20 CP @ 0°C

Hazardous Air Pollutants (1)	Vapor Viscosity Micropoises	Liquid Viscosity Centipoise
Hexane	68 MP @ 25°C	.31 CP @ 25°C
Hydrazine	86 MP @ 25°C	.92 CP @ 25°C
Hydrogen sulfide (2)	120 MP @ 0°C	
Methanol	98 MP @ 25°C	.55 CP @ 25°C
Methyl bromide (Bromoethane)	124 MP @ 25°C	.32 CP @ 20°C
Methyl chloride (Chloromethane)	108 MP @ 20°C	.19 CP @ 20°C
Methyl chloroform (1,1,1-Trichloroethane)	93 MP @ 25°C	.80 CP @ 25°C
Methyl ethyl ketone (MEK) (2-Butanone)	73 MP @ 25°C	.41 CP @ 25°C
Methyl isobutyl ketone MIBK (Hexone)	67 MP @ 25°C	.57 CP @ 25°C
Methyl methacrylate	70 MP @ 25°C	.53 CP @ 25°C
Methyl chloride (Dichloromethane)	97 MP @ 20°C	.45 CP @ 20°C
Phosgene	118 MP @ 20°C	.39 CP @ 20°C
Propionaldehyde	78 MP @ 25°C	.36 CP @ 25°C
Propylene dichloride (1,2-Dichloropropane)	74 MP @ 20°C	.86 CP @ 20°C
Propylene oxide	90 MP @ 25°C	.37 CP @ 25°C
Styrene	65 MP @ 25°C	.70 CP @ 25°C
Toluene	70 MP @ 25°C	.55 CP @ 25°C
Trichloroethylene	93 MP @ 20°C	.60 CP @ 20°C
Triethylamine TEA	73 MP @ 50°C	.39 CP @ 20°C
Vinyl acetate	80 MP @ 25°C	.43 CP @ 20°C
Vinyl chloride	107 MP @ 20°C	.19 CP @ 20°C
Vinylidene chloride (1,1-Dichloroethylene)	199 MP @ 20°C	.48 CP @ 20°C
Xylenes (Isomers and mixers) (*M & P Xylene, **O-Xylene)	65 MP @ 25°C	*.58 CP @ 25°C **.79 CP @ 25°C

1) Viscosities from Gallant Series, "Physical Properties of Hydrocarbons", published in Hydrocarbon Processing and Petroleum Refiners (various issues) unless otherwise noted.  
2) "A Treatise on Leakage" - Henry Vogt Machine Company technical paper. 3) "Chlorine Manual", 1972 printing, Chlorine Institute.

# Fugitive Emissions: A Leakage Viewpoint

**TABLE 1A**

**Parts per Million Leakage (Volumetric)**

**PPM(v) (2)**

Size (Spherical)	Volume (1) Drop/Bubble	Theoretical Leak Rate PPM(v) (3)										
		Bubbles per Minute										
Drop or Bubble Diameter	In <sup>3</sup>	4	5	6	8	10	16	20	25	32	50	64
1.32"	1.598 x 10 <sup>-5</sup>	9.5	0.6	0.8	1.0	1.3	2.1	2.6	3.3	4.2	6.5	8.4
1/16"	1.278 x 10 <sup>-4</sup>	4.2	5.2	6.3	8.4	10	17	21	26	34	52	67
3/32"	4.314 x 10 <sup>-4</sup>	14	18	21	28	35	57	71	88	113	177	226
1/8"	1.023 x 10 <sup>-4</sup>	34	42	50	67	84	134	168	210	268	419	536
5/32"	1.997 x 10 <sup>-3</sup>	65	82	98	131	164	262	327	409	524	818	1047
3/16"	3.451 x 10 <sup>-3</sup>	113	141	170	226	283	452	566	707	905	1414	1810

1) Volume of bubble =  $\frac{\pi}{6}$  (diameter)<sup>3</sup>

2) Theoretical PPM(v) leak rate based on introducing the comparable bubble leak volume of a 100% methane gas into a pipe flowing pure air at 2 liters/minute.

3) PPM = 491642 x leak rate (SCIS) @ 2 liters minute flow rate.

For flow rates larger than 2 liters/minute the PPM would be proportionally smaller.

For flow rates smaller than 2 liters/minute the PPM would be proportionally larger.



**Vogt Valves**

1511 Jefferson Street  
Sulphur Springs, TX 75482

**US Sales Offices**

Phone: 903-885-3151  
Fax: 903-439-3386

**Toll-Free Telephone Service**

1-800-225-6989

**Visit Our Website**

[www.flowserve.com](http://www.flowserve.com)

**After Hours Customer Service**

1-800-543-3927

Flowserve Corporation has established industry leadership in the design and manufacture of its products. When properly selected, this Flowserve product is designed to perform its intended function safely during its useful life. However, the purchaser or user of Flowserve products should be aware that Flowserve products might be used in numerous applications under a wide variety of industrial service conditions. Although Flowserve can (and often does) provide general guidelines, it cannot provide specific data and warnings for all possible applications. The purchaser/user must therefore assume the ultimate responsibility for the proper sizing and selection, installation, operation, and maintenance of Flowserve products. The purchaser/user should read and understand the Installation Operation Maintenance (IOM) instructions included with the product, and train its employees and contractors in the safe use of Flowserve products in connection with the specific application.

While the information and specifications contained in this literature are believed to be accurate, they are supplied for informative purposes only and should not be considered certified or as a guarantee of satisfactory results by reliance thereon. Nothing contained herein is to be construed as a warranty or guarantee, express or implied, regarding any matter with respect to this product. Because Flowserve is continually improving and upgrading its product design, the specifications, dimensions and information contained herein are subject to change without notice. Should any question arise concerning these provisions, the purchaser/user should contact Flowserve Corporation at any one of its worldwide operations or offices.

For more information about Flowserve Corporation, contact [www.flowserve.com](http://www.flowserve.com) or call USA 1-800-225-6989.

**FLOWSERVE CORPORATION**

**FLOW CONTROL DIVISION**

**Vogt Valves**

1511 Jefferson Street  
Sulphur Springs, TX 75482  
Phone: 903-885-3151  
Facsimile: 903-439-3386